1. Mass Conservation

 $\frac{dm}{dr} = 4\pi r^2 \rho$ 

dr  $\frac{1}{dm} - \frac{1}{4\pi r^2 \rho}$ 

eulerian

lagrangian

2. Hydrostatic Equilibrium





eulerian

lagrangian

Need equation of state:

$$P = f(\rho, T, X_i)$$

3. Energy Generation

 $\frac{dL_r}{dr} = 4\pi r^2 \rho \varepsilon$ 

 $\frac{dL_m}{dm} = \varepsilon$ 

eulerian

lagrangian

Need nuclear physics:

$$\varepsilon = f(\rho, T, X_i)$$

4. Energy Flow: Radiation



eulerian

lagrangian

Need opacity:

$$\kappa = f(\rho, T, X_i)$$

4. Energy Flow: Convection

$$\frac{dT}{dr} = -\left(1 - \frac{1}{\Gamma_2}\right)\frac{Gm\rho T}{r^2 P} \quad \frac{dT}{dm} = -\left(1 - \frac{1}{\Gamma_2}\right)\frac{GmT}{4\pi r^4 P}$$

eulerian

lagrangian

Need adiabatic exponent:

$$\Gamma_2 = f(\rho, T, X_i)$$

Equation of State (non-degenerate matter)

$$P = \frac{1}{3}aT^4 + \frac{N_Ak}{\mu}\rho T$$

Mean molecular weight:

$$\frac{1}{\mu} = \frac{1}{\mu_i} + \frac{1}{\mu_e} = \sum_i \frac{X_i}{A_i} + \sum_i \frac{Z_i X_i y_i}{A_i}$$

Ionization fractions y<sub>i</sub>

Saha equation :

$$\frac{n^{+}n_{e}}{n^{0}} = \frac{2G^{+}}{G^{0}} \frac{\left(2\pi m_{e}kT\right)^{3/2}}{h^{3}} \exp\left(-\frac{\chi}{kT}\right)$$

e.g., Hydrogen only : \_\_\_\_

$$\frac{y^2}{1-y} = \frac{1}{N_A \rho} \frac{\left(2\pi m_e kT\right)^{3/2}}{h^3} \exp\left(-\frac{\chi_H}{kT}\right)$$

Thermodynamics

Adiabatic index :

$$\frac{\Gamma_2}{\Gamma_2 - 1} = \left(\frac{\partial \ln P}{\partial \ln T}\right)_{ad}$$

$$\Gamma_2 = \frac{32 - 24\beta - 3\beta^2}{24 - 18\beta - 3\beta^2} \qquad \beta = \frac{P_g}{P_{tot}}$$

(assuming neutral or fully ionized gas)

**Opacity:** approximations

$$\frac{1}{\kappa} \approx \frac{1}{\kappa_{H^{-}}} + \frac{1}{\kappa_{e} + \kappa_{ff} + \kappa_{bf}}$$

 $\kappa_e = 0.2(1+X)cm^2g^{-1}$ 

(assuming fully ionized and no metals)

$$\kappa_{ff} \approx 4 \times 10^{22} (X+Y)(1+X) \rho T^{-3.5} cm^2 g^{-1}$$

$$\kappa_{bf} \approx 4 \times 10^{25} Z (1+X) \rho T^{-3.5} cm^2 g^{-1}$$

$$\kappa_{H^{-}} \approx 2.5 \times 10^{-31} (Z/0.02) \rho^{1/2} T^9 cm^2 g^{-1}$$

**Opacity: tables** 



Convection

Convection happens when:



$$L_m > \frac{16\pi acG}{3\kappa_R} \left(1 - \frac{1}{\Gamma_2}\right) \frac{T^4 m}{P}$$

**Energy generation** 

$$\varepsilon = \varepsilon_{pp} + \varepsilon_{CNO} + \varepsilon_{3\alpha}$$

$$\varepsilon_{pp} = 2.4 \times 10^4 \frac{\rho X^2}{T_9^{2/3}} \exp(-3.38/T_9^{1/3}) ergs^{-1}g^{-1}$$

$$\varepsilon_{CNO} \approx 4.4 \times 10^{25} \frac{\rho XZ}{T_9^{2/3}} \exp\left(-15.228/T_9^{1/3}\right) ergs^{-1}g^{-1}$$

$$\varepsilon_{3\alpha} = 5 \times 10^8 \frac{\rho^2 Y^3}{T_9^3} \exp(-4.4/T_9) ergs^{-1}g^{-1}$$

Given M and X,Y,Z, solve structure equations



to get r, P, T, L<sub>m</sub> as a function of m

Need to know:

 $\rho(P,T,X,Y,Z)$   $\kappa_{R}(\rho,T,X,Y,Z)$ 

 $\varepsilon(\rho,T,X,Y,Z)$  $\Gamma_2(\rho,T,X,Y,Z)$ 





Some of these equations are indeterminant at center.

It is better to start the integration at a very small m>0.

Central boundary conditions

At a very small m>0:

$$r \neq 0$$
  $m = \frac{4}{3}\pi r^3 \rho_c \rightarrow r = \left(\frac{3m}{4\pi\rho_c}\right)^{1/3}$ 

$$L_m \neq 0$$
  $L_m = \varepsilon_c m$ 

Central boundary conditions

• We can get boundary conditions for P and T by expanding and demanding that their derivatives are zero at r=0

 $P(r) = P(0) + P'(0)(r-0) + \frac{1}{2}P''(0)(r-0)^{2}$  $=P_c+P''(0)\frac{r^2}{2}$  $P(r) = P_c - \frac{2}{3}\pi G\rho_c^2 r^2$  $P'(r) = -\frac{Gm\rho}{r^2}$  $= -\frac{G\rho}{r^2} \left(\frac{4}{3}\pi r^3 \rho_c\right) = -\frac{4}{3}\pi G\rho_c^2 r$ 

Central boundary conditions

• Similarly,

$$T(r) = T(0) + T'(0)(r-0) + \frac{1}{2}T''(0)(r-0)^{2}$$

$$= T_{c} + T''(0)\frac{r^{2}}{2}$$

$$T(r) = T_{c} - \frac{\kappa_{c}\rho_{c}^{2}\varepsilon_{c}}{8acT_{c}^{3}}r^{2}$$

$$T'(r) = -\frac{3\kappa_{R}\rho L_{r}}{16\pi acr^{2}T^{3}}$$

$$T(r) = T_{c} - \frac{\kappa_{c}\rho_{c}^{2}\varepsilon_{c}}{8acT_{c}^{3}}r^{2}$$

$$T'(r) = \left(1 - \frac{1}{\Gamma_{2}}\right)\frac{T}{P}\frac{dP}{dr}$$

$$T(r) = T_{c} - \left(1 - \frac{1}{\Gamma_{2,c}}\right)\frac{2\pi G\rho_{c}^{2}T_{c}}{3P_{c}}r^{2}$$

Surface boundary conditions

We can do better than T=P=0 at surface. ٠

guess R and L:

$$L = 4\pi R^2 \sigma T_s^4 \rightarrow T_s = \left(\frac{L}{4\pi R^2 \sigma}\right)^{1/4}$$

/

Guess  $\rho$ very small, e.g., 10-5 g cm-3:

$$P_s = \frac{1}{3}aT_s^4 + \frac{N_Ak}{\mu}\rho_s T_s$$

#### Steps in constructing a stellar model

- 1. Compute  $\rho$ ,  $\kappa$ , s, g, fu, fu
  - Beware of P dropping below OPACITY
  - Use approximations for crude results
  - Interpolate using tables (use approximations outside table bounds) <u>ENERGY GENERATION</u>
  - Use formulas for pp, CNO, and 3

#### THERMODYNAMICS

- 5/3 for ideal gas, 4/3 for radiation pressure
- departs from these values when
  - Mixture of ideal gas and radiation lpha
  - Ionization zones

$$\begin{array}{c} \Gamma_2 = \\ \Gamma_2 \end{array}$$

P, T, X, Y, Z

#### Steps in constructing a stellar model

- 2. Use four structure equations to compute given stanting values VS. for these (boundary conditions). m
  - Given values of at shell ٠ compute 4 derivatives:
  - Use these derivatives to compute  $P, T, L_m, \rho, \kappa, \varepsilon, \Gamma_2$ ٠ at shell  $\frac{dr}{dm}, \frac{dP}{dm}, \frac{dL_m}{dm}, \frac{dT}{dm}$

e.g.,

near center and surface. Shell size ٠ r P T I

$$i+1$$

$$r[i+1] = r[i] + \left(\frac{dr}{dm}\right)[i] \times dm$$

$$dm < 10^{-4} M$$

am < 10

#### Steps in constructing a stellar model

- 3. Deal with lack of complete boundary conditions at center or surface.
  - At center, have r, L<sub>m</sub>, but not P, T
  - At surface, have P, T, but not r, L<sub>m</sub>
  - General approach: guess values for missing conditions at one end, run model, and compare boundary conditions at other end.
     <u>PROBLEM</u>: small changes in conditions at center can cause large differences at surface → difficult to reach convergence.
     <u>SOLUTION</u>: Shoot from both center and surface and meet halfway through star.



- Guess values for and  $T_c$  and integrate outwards from  $m \stackrel{\text{to}}{=} 0$  m = M/2
- Guess values for and R nd integrate inwards from to  $m = M \qquad m = M/2$
- Compute discrepancies  $\Delta r, \Delta P, \Delta T, \Delta L_m \qquad m = M/2$

• Work in log space:  $\log P$ ,  $\log T$ ,  $\log r$ ,  $\log L_m$ 







• Repeat using new trial values:

 $(\log T_c - d \log T_c)$  and  $(\log T_c + d \log T_c)$  with  $\log P_c$ ,  $\log R$ ,  $\log L$  $(\log P_c - d \log P_c)$  and  $(\log P_c + d \log P_c)$  with  $\log T_c$ ,  $\log R$ ,  $\log L$  $(\log R - d \log R)$  and  $(\log R + d \log R)$  with  $\log P_c$ ,  $\log T_c$ ,  $\log L$  $(\log L - d \log L)$  and  $(\log L + d \log L)$  with  $\log P_c$ ,  $\log T_c$ ,  $\log R$ 

• Compute new discrepancies in each case.

 $\Delta \log r$ ,  $\Delta \log P$ ,  $\Delta \log T$ ,  $\Delta \log L_m$ 

• Get 16 derivatives. e.g.,

$$\frac{\partial (\Delta \log r)}{\partial \log P_c} = \frac{(\Delta \log r)_{\log P_c + d \log P_c} - (\Delta \log r)_{\log P - d \log P_c}}{2d \log P_c}$$

• Use these derivatives to calculate improved boundary conditions.

$$\log P'_{c} = \log P_{c} + \delta \log P_{c}$$
$$\log T'_{c} = \log T_{c} + \delta \log T_{c}$$
$$\log R' = \log R + \delta \log R$$
$$\log L' = \log L + \delta \log L$$

• General idea:

$$-\Delta \log r = \delta \log P_c \frac{\partial (\Delta \log r)}{\partial \log P_c} \rightarrow \delta \log P_c = -\Delta \log r \left[ \frac{\partial (\Delta \log r)}{\partial \log P_c} \right]^{-1}$$

• More complicated with 4 variables!



 Invert matrix to solve for (actually take smaller steps ~0.1x)  $\delta \log P_c$ ,  $\delta \log T_c$ ,  $\delta \log R$ ,  $\delta \log L$ 

 Iterate until convergence is reached: discrepancies vanish (i.e., drop below a threshold value)